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A gas turbine combustion chamber modeling by physical model

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ABSTRACT

The validity of the gas turbine unit model largely depends on the accuracy of the flue gas temperature value calculation at the gas turbine inlet (TIT). This temperature is determined by the maximum combustion temperature. In variable running mode, the temperature value is regulated by changing the ratio of air and fuel at the inlet to the combustion chamber. The paper presents a model of a gas turbine combustion chamber using Modelica, an object-oriented language for modeling complex physical systems with the aim of determining the temperature of combustion flue gases, specific heat capacity, enthalpy, and flue gas composition at different gas turbine loads.

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1 Introduction

The combustion chamber is an important link in the modeling of a gas turbine unit. The exhaust gas values from the gas turbine and their magnitude outlet from the combustion chamber affects the accuracy of the calculation of the entire gas turbine model. In cases of modeling a heat turbine due to the complexity of the combustion temperature calculation, it is often assumed that the flue gas temperature at the outlet of the combustion chamber is an isotherm which is not the case in reality and leads to inaccurate values in the calculation. As efficiency of the entire gas turbine process depends largely on the combustion process in the combustion chamber, many researches were conducted in that direction. Railckas et al., [1] carried out CFD simulations to see the operation of a gas turbine combustion chamber with the STAR-CCM software where they compared simulation results with the operating parameters of the actual process. Comparison results are in the congruence with the actual running gas turbine. The transient combustion models were simulated by Large Eddy Simulations (LES) data, [2]. Combustion model in that study descripts turbulent premixed combustion, which is encountered at the injector exit of gas turbines combustor, by using the Coherent Flame Model (CFM) formalism, where tried to increase the range of validity of this 0D combustion model to a high number of aero engine combustor geometries, but without satisfactory results in the turbulence and the vortex definition. The turbulence models were modelled successfully by a URANS formulation in [3], using the SST turbulence model, as the basic modelling approach. The numerical results obtained by different turbulence models are comparable with the overall performance and have a fair overall agreement with the experimental data, what is their validation. The combustion chambers are components which produce the highest destruction rate in open cycle gas turbines [4, 5]. The similar conclusion can be found in [6] for closed cycle gas turbines where the highest destruction rate occurs in main heater (or more of them). All of the combustion (or heat exchange) processes in gas or steam turbines can be improved and optimized by using various machine learning methods [7-10]. The advantage of these approaches is in very low relative error in comparison with the available data.

For the purpose of calculating the combustion temperature, it is necessary to use thermodynamic data which are described by interpolation curves of specific heat capacity and enthalpy which are known in the literature [11-13] and are often used for modeling purposes. These functions describe the properties of combustion participants with sufficient accuracy. As the range of interpolated values covers the temperature ranges of 300-1000 and 1000-5000 K these interpolations show large deviations in the calculation of the flue gas temperature in the combustion chamber of the gas turbine, which can be up to 100 K. The reason for this phenomenon lies in the fact that the temperature range of combustion chambers are in the interval of 900-1250 K which just falls between these two intervals. To address this problem they were made on the basis of data [14] new interpolation curves (Table 1 and Table 2) with a higher degree of accuracy and based on them a combustion chamber model was made which in the iterative procedure calculates the combustion temperature flue gas composition, specific heat capacity, average flue gas heat capacity and enthalpy of the exhaust gases.

2 The combustion participants thermodynamic properties

Gases that occur in the process of complete combustion are CO_2 , H_2O (g), N_2 , O_2 which values are coefficients for calculating the heat capacity and enthalpy of gases given in Tables 1 and 2. The enthalpy of combustion gases (flue gases) is calculated by expression:

$$h(T) = \int_{T_0}^{T} c_p dT \tag{1}$$

where heat capacities in the Table 1 are calculated by:

$$c_p(T) = a_1 + a_2 T \tag{2}$$

where heat enthalpy in the Table 2 are calculated by:

$$h(T) = a_1 + a_2 T + a_3 T^2 (3)$$

Table 1 Combustion gases heat capacity coefficients

		220-800 K	800-1500 K	1500-2500 K
CO ₂	a ₁	0,02913557	4,45264E-02	0,052758903
	a ₂	2,99640E-05	9,70935E-06	3,70306E-06
H ₂ 0 _(g)	a ₁	3,03695E-02	2,90995E-02	3,72788E-02
	a ₂	9,93150E-06	1,21192E-05	6,83606E-06
N ₂	a ₁	2,76147E-02	2,77732E-02	3,24244E-02
	a ₂	4,23709E-06	4,90748E-06	1,75613E-06
0,	a ₁	2,65373E-02	3,08985E-02	3,30255E-02
	a ₂	9,17537E-06	3,93738E-06	2,37424E-06

Source: Authors

Table 2 Combustion gases enthalpy coefficients

		220-800 K	800-1500 K	1500-2500 K
	a_1	-6,35634E-01	-6,35634E-01	-1,21288E+01
CO ₂	a_2	2,91356E-02	4,45264E-02	5,27589E-02
	a_3	1,49820E-05	4,85467E-06	1,85153E-06
	a ₁	4,02478E-01	7,31029E-01	-5,64619E+00
$H_2O_{(g)}$	a_2	3,03695E-02	2,90995E-02	3,72788E-02
	a_3	4,96575E-06	6,05960E-06	3,72788E-02
	a_1	2,42385E-01	-9,06821E-02	-3,55367E+00
N_2	a_2	2,76147E-02	2,77732E-02	3,24244E-02
	a_3	2,11854E-06	2,45374E-06	8,78063E-07
	a_1	3,57855E-01	-1,47096E+00	-2,92248E+00
02	a_2	2,65373E-02	3,08985E-02	3,30255E-02
	a_3	4,58768E-06	1,96869E-06	1,18712E-06

Source: Authors

3 The control volume of the combustion chamber

As the adiabatic combustion temperature can be over 2200 K [15] on the example of Methane, $\mathrm{CH_4}$ $\Phi=1$ is $T_{\mathrm{adiabatic}}=2267.2$ K [16]. Such high amounts of temperature at the outlet of the combustion chamber would cause damage to the gas turbine blades especially on gas models turbines of lower power (up to 5 MW) which do not have blade cooling implemented. The solution to this the problem can be obtained by bringing 3 to 6 time larger amount of air than required by stoichiometric calculation [17], in order to maintain the inlet temperature of the gas turbine (TIT) as high enough as to allow optimally turbine power at which the turbine blades will not be destroyed.

Adiabatic combustion temperature $T_{\rm adiabatic}$ the maximum flue gas temperature inside combustion chambers [18].

3.1 Adiabatic temperature calculation, $T_{\text{adiabatic}}$

By applying the first law of thermodynamics to the control volume of the combustion chamber it may be written [19]:

$$Q - W = H_{P} - H_{R} =$$

$$= \sum_{P} N_{i} (h_{f}^{o} + h - h^{o})_{i} - \sum_{R} N_{i} (h_{f}^{o} + h - h^{o})_{i}$$
(4)

where enthalpy of product and reactants of combustion is:

$$h(T) = h_{\varepsilon}^{\circ}(T^{\circ}) + h(T) - h^{\circ}(T^{\circ}) \tag{5}$$

The enthalpy of formation $h_f^{\,\circ}$ for the standard reference state (SRS) is taken at 25 °C and 0,1013 MPa. General equation of hydrocarbon combustion is:

$$\underbrace{C_x H_y + \left(x + \frac{y}{4}\right) O_2}_{\text{fuel + oxygen}} \rightarrow \underbrace{xCO_2 + \left(\frac{y}{2}\right) H_2 O}_{\text{flue gas}} \tag{6}$$

The first part of equation 6 is reaction of fuel and oxygen and the other part are exhaust gases. General equation of hydrocarbon combustion from the air:

$$\underbrace{C_x H_y + aO_2 + 3.7aN_2}_{\text{fuel + air}} \rightarrow \underbrace{xCO_2 + \left(\frac{y}{2}\right)}_{\text{flue gas}} H_2O + 03.76aN_2 \tag{7}$$

The stoichiometric ratio of air and fuel can be written as:

$$(A/F)_s = \left(\frac{m_a}{m_f}\right)_c \tag{8}$$

The relative ratio is the ratio of the mixture of air and fuel and the stoichiometric mixture of air and fuel:

$$\lambda = \frac{(A/F)}{(A/F)_s} \tag{9}$$

A commonly used quantity in practice is the equivalent ratio:

$$\Phi = \frac{1}{\lambda} = \frac{(A/F)_s}{(A/F)} = \frac{(F/A)}{(F/A)_s}$$
 (10)

Based on the volume amounts from the air mixture whereby there is 21% $\rm O_2$ and 79% $\rm N_2$ in the air it can be written [20], that the stoichiometric mixture of air and fuel then amounts:

$$(A/F)_s = \left(\frac{m_a}{m_f}\right)_s = \frac{4.76\left(x + \frac{y}{4}\right)}{1} \cdot \frac{M_a}{M_f} \tag{11}$$

where M_{α} is molecular air mass and M_{α} is molecular fuel mass.

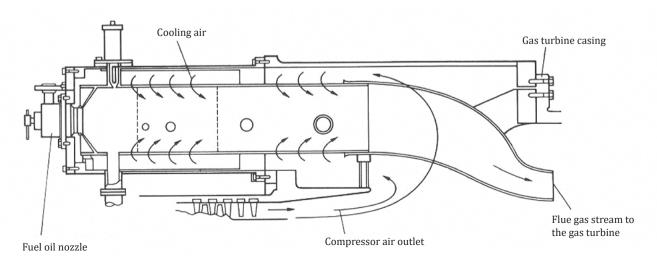


Figure 1 Gas turbine combustion chamber [17]

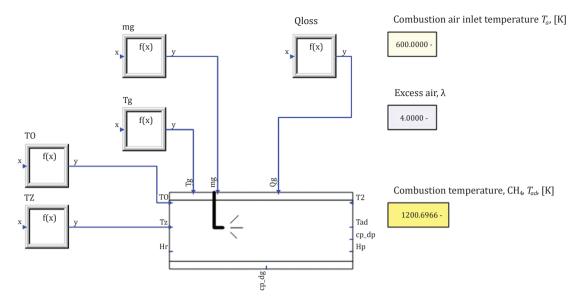


Figure 2 Modelica the combustion chamber model

Source: Authors

3.2 Nonlinear algebraic combustion equation

The adiabatic combustion process is described by the nonlinear algebraic equation f(T) = 0. The procedure for solving this equation is based on the "Regula falsi" method or the secant method [21]. In the procedure it is necessary to perform an iteration in which the temperature T which will be found corresponds to the adiabatic combustion temperature a which represents the zero point of the function. Iteration procedure is based on the iterative scheme described by the equation:

$$T_{i+1} = \frac{T_{i-1}f(T_i) - T_i f(T_{i-1})}{f(T_i) - f(T_{i-1})}$$
(12)

in which the index *i* represents an iterative step. The iteration procedure is repeated until it is not satisfied convergence criterion, taking the values of the unknowns calculated from of the previous step

$$\left| \frac{T_{i+1} - T_i}{T_i} \right| \le \varepsilon \tag{13}$$

4 Modelling and simulation

The paper presents a model of a gas turbine combustion chamber using Modelica language, for modeling complex physical systems with the aim of determining the temperature of combustion flue gases, specific heat capacity, enthalpy, and flue gas composition at different gas turbine loads.

Modelica [22] is an open standard for describing physical models and their components, whose is a core object-oriented language, which is suitable for describing

complex physical systems from areas such as mechanics, electrical engineering, hydraulics and thermodynamics. The special interest is in the area of the separate production of heat energy from a boiler and cooling energy from a compression refrigeration unit. These are powered with electrical energy from an external network which could be replaced with a CCHP system (combined cooling, heating and power - combined cooling, heating and electricity generation) based on the operation of a gas turbine and absorption refrigeration unit [23, 24]. The mentioned models are given to be described by differential-algebraic equations (DAE). Models described by differential algebraic equations are solved by applying different numerical methods (Euler, Runge - Kutta Dassl). Basing language development and ownership on open source principles has encouraged many manufacturers to develop and implement different versions of Modelica Simulation Environments as OpenModelica [25], MapleSim [26], Wolfram SystemModeler [27], SimulationX [28].

5 Analysis results and validation

The Modelica, results of simulations of the combustion chamber model (Table 3 and Figure 3) of CH_4 , for variated values relative ratio λ and inlet air temperature to the combustion chamber of 600 K compared to the CHEMCAD [29] and Cantera [30] tool. The CHEMCAD is an integrated suite of intuitive chemical process simulation software that fits into the chemical engineering workflow and supercharges an engineer's efficiency. CHEMCAD combustion chamber tool uses mode of "Gibbs free energy reactor". The CERFACS, [31] is Cantera based Adiabatic Flame Temperature Calculator based on the object-oriented software toolkit for chemical kinetics, thermodynamics,

 $T_{ad}(K)$ Φ **MODELICA CHEMCAD CERFACS** λ T_a(K) 3 0,3333 600 1.375,87 1.379,99 1391,98 3,5 0,2857 600 1.277,10 1.265,12 1291,53 4 0,2500 600 1.200,70 1.203,79 1213,82 4,5 0,2222 600 1.139,85 1.130,15 1151,84 5 0,2000 600 1.090,25 1.081,42 1101,38 0,1818 1.049,05 1.040,94 1059,36 5,5 600

Table 3 Comparative results of adiabatic combustion temperature simulation

Source: Authors

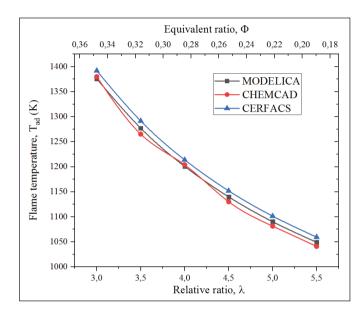


Figure 3 Values of adiabatic flame temperature as a function relative ratio λ

Source: Authors

and transport processes. The code utilizes object-oriented concepts for robust yet flexible phase models, and algorithms are generalized so that users can explore different phase models with minimal changes to their overall code. Currently, Cantera can be used from Python and MATLAB, or in applications written in C/C++ and Fortran 90. Cantera also provides a limited number of solvers for time-dependent reactor networks and steady one-dimensional reacting flows.

6 Conclusion

The validity of the gas turbine unit model largely depends on the accuracy of the flue gas temperature value calculation at the gas turbine inlet (TIT). This temperature is determined by the temperature of the flame in the combustion chamber. In variable running mode, the temperature value is regulated by changing the air to fuel ratio at the inlet to the combustion chamber. Application of Modelica in the development of a model of the control

volume of the combustion chamber of a gas turbine, shows excellent results which allow to make a valid model of a gas turbine unit. Modelica main task is to calculate the combustion temperature of flue gases and the size and volume fraction of individual combustion participants and simulation of combustion chamber operation validated with equipment manufacturer values tools. As the real data for such simulated processes is difficult to collect due to limited research budget the validation of the Modelica (SimulationX) computed values were compared and validated by combustion process simulation with CHEMCAD and CERFACS (Cantera).

Nomenclature

Abbreviation

SRS	Standard reference state	
TIT	Temperature of exhaust gases at gas	[K]
	turhine inlet	

Latin symbols

till Syl	1110013	
Α	Air	
F	Fuel	
h	Enthalpy	[kJ/kmol]
ṁ	Mass flow rate	[kg/s]
M	Molar mass	[kg/kmol]
N	Plural substance	
r	Volume ratio	[%]
Q	Power	[kW]
T	Temperature	[K]
-		

Greek symbols

Φ Equivalent ratio

λ Relative ratio

Index

lex	
a	Air
ad	Adiabatic
f	Fuel
fo	Formation
g	Gas
0	Reference
P	Product
R	Reactant

stoichiometric

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